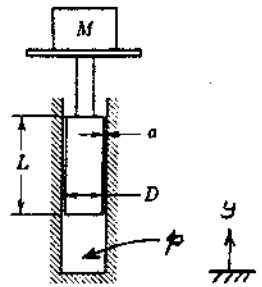


Problem 8.15

Given: Piston-cylinder device, as shown.

$$D = 6 \text{ mm} \quad L = 25 \text{ mm}$$

Liquid is SAE-30 oil at 20°C.



- Find: (a) M to develop $p = 1.5 \text{ MPa (gage)}$
 (b) Leakage flow rate in terms of a
 (c) Maximum a to provide $< 1 \text{ mm/min}$ movement.

Solution: The mass may be found from a force balance on the piston.

$$\Sigma F_y = \frac{\pi D^2}{4} (p - p_{atm}) - Mg = 0 \quad \text{so } M = \frac{\pi D^2}{4g} p_{\text{gage}}$$

$$M = \frac{\pi}{4} \times (0.006)^2 \text{ m}^2 \times 1.5 \times 10^6 \frac{\text{N}}{\text{m}^2} \times \frac{\text{s}^2}{9.81 \text{ m}} \times \frac{\text{kg} \cdot \text{m}}{\text{N} \cdot \text{s}^2} = 4.32 \text{ kg}$$

The leakage flow rate may be evaluated for flow between flat plates. From Eq. 8.6c, neglecting motion of the piston,

$$\frac{Q}{L} = \frac{a^3 \Delta p}{12 \mu L} \quad \text{or, since } l = \pi D, \quad Q = \frac{\pi a^3 \Delta p D}{12 \mu L} \sim a^3$$

The piston, moving downward at speed, v , displaces liquid at rate

$$Q = \frac{\pi D^2}{4} v = \frac{\pi}{4} (0.006)^2 \text{ m}^2 \times 0.001 \frac{\text{m}}{\text{min}} \times \frac{\text{min}}{60 \text{ s}} = 4.71 \times 10^{-10} \text{ m}^3/\text{s}$$

Then, with $\mu = 0.42 \text{ N} \cdot \text{sec}/\text{m}^2$ (at 20°C, Fig. A.2),

$$a = \left[\frac{12 \mu Q L}{\pi D \Delta p} \right]^{1/3} = \left[\frac{12 \times 0.42 \frac{\text{N} \cdot \text{s}}{\text{m}^2} \times 4.71 \times 10^{-10} \frac{\text{m}^3}{\text{s}} \times 0.025 \text{ m} \times \frac{1}{0.006 \text{ m}} \times \frac{\text{m}^2}{1.5 \times 10^6 \text{ N}} \right]^{1/3}$$

$$a = 1.28 \times 10^{-5} \text{ m} \quad (12.8 \mu\text{m})$$

Check assumptions: $\bar{v} = \frac{Q}{A} = \frac{Q}{\pi D a} = \frac{1}{\pi} \times 4.71 \times 10^{-10} \frac{\text{m}^3}{\text{s}} \times \frac{1}{0.006 \text{ m}} \times \frac{1}{1.28 \times 10^{-5} \text{ m}} = 1.95 \frac{\text{mm}}{\text{s}}$

Thus $\frac{\bar{v}}{v} = \frac{1 \text{ mm}}{\text{min}} \times \frac{\text{sec}}{1.95 \text{ mm}} \times \frac{\text{min}}{60 \text{ s}} = 0.00855 < 0.01$

Therefore piston motion is negligible.

Also $Re = \frac{\bar{v} a}{\nu}$; $\nu = \frac{\mu}{\rho} = \frac{\mu}{Sg \rho_{\text{oil}}}$. From Table A.2 (Appendix A), $Sg = 0.92$

$$\nu = 0.42 \frac{\text{N} \cdot \text{s}}{\text{m}^2} \times \frac{\text{m}^3}{(0.92) 1000 \text{ kg}} \times \frac{\text{kg} \cdot \text{m}}{\text{N} \cdot \text{s}^2} = 4.57 \times 10^{-4} \text{ m}^2/\text{s}$$

$$Re = 1.95 \times 10^{-3} \frac{\text{m}}{\text{s}} \times 1.28 \times 10^{-5} \text{ m} \times \frac{\text{s}}{4.57 \times 10^{-4} \text{ m}^2} = 5.46 \times 10^{-5} \ll 1$$

Therefore flow is surely laminar!

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